

Gasification Technology: A Review of Technical Aspects

Mugdha Bhamare ¹, Kailasnath B. Sutar ¹

¹ *Department of Mechanical Engineering, Bharati Vidyapeeth (Deemed to be University),
College of Engineering, Pune, India-411043*

Abstract

Gasification technology is a greener alternative to traditional fossil fuel-based energy generation, showing great promise as a sustainable solution for waste management and energy production. This method produces synthesis gas (syngas), which is made up of hydrogen, carbon monoxide, and trace amounts of other gases, from a variety of carbon-containing feedstocks, including coal, biomass, and municipal solid waste. Syngas can be used to produce fuels and useful chemicals, as well as to generate heat and electricity.

An overview of gasification technology is given in this abstract, with emphasis on its main ideas, advantages, and uses. High efficiency, lower greenhouse gas emissions, and the capacity to handle a variety of feedstocks are just a few benefits of gasification.

By reducing the environmental impact of landfills and turning organic waste materials into syngas, gasification serves a critical role in waste management in addition to delivering electricity. The significance of ongoing research and development in gasification technology is brought out in the abstract's conclusion in order to maximize its effectiveness, raise its financial long-term viability and broaden its applications. To fully utilize gasification and open the door to a more environmentally friendly and sustainable energy future, cooperation between researchers, business executives, and policymakers is crucial.

Keywords: Gasification technology, Syngas, Energy production, Waste management, Sustainability, Feedstocks.

1. Introduction

The introduction section provides an overview of gasification technology, highlighting its historical evolution, key principles, and the importance of syngas production in the context of renewable energy sources and sustainable development. Biomass, a term got from "natural mass," alludes to natural materials, prevalently plant and creature build-ups that can be used as a sustainable wellspring of energy. This diverse category encompasses a wide range of

biological materials, including wood, crop residues, agricultural by-products, and organic waste from households and industries. Unlike fossil fuels, biomass is considered a renewable energy source because the organic matter it comprises can be replenished over relatively short periods through natural processes. Legislators and lawmakers, in light of natural issues, vacillations in fossil incomes, and the rising interest for energy in the advanced world, have pushed for the utilization of option non-fossil energy sources, especially sustainable assets [1,2,3].

Lignocellulosic biomass, as the most abundant source of renewable carbon that does not contribute to global warming, is particularly significant considering the limited supplies of traditional fossil fuels [4,5,6]. One of the most feasible pathways to meet future fuel and chemical needs is the development of new technologies that incorporate biomass in the production of renewable energy.

Gasification, one of the promising advances for creating fuel and energy from biomass, includes the corruption of biomass. Responding the material at high temperatures (>700 °C) with a controlled measure of oxidizing specialist (air, oxygen, or/and steam) brings about this cycle. Kirubakaran revealed the creation of carbon monoxide, hydrogen, methane, and carbon dioxide. Different models, including thermodynamic balance, motor, computational liquid elements (CFD), counterfeit brain organization (ANN), and ASPEN In addition to models, have been utilized for recreating the gasification cycle in both downdraft and updraft gasifiers. The use of biomass for energy regularly includes the thermochemical change process, creating vaporous, fluid, and strong energizes as wanted items. Past exploration, expecting to enhance the gasification cycle, has led trial examinations as well as essentially utilized mathematical methodologies. Mathematical models created utilizing Computational Liquid Elements (CFD) codes, like ANSYS Familiar and ANSYS CFX programming, have been instrumental. Reenactment results from this mathematical methodology can help with advancing framework plan and activity, giving bits of knowledge into the unique cycles inside the reactor. Late demonstrating endeavors have zeroed in on the thermo-compound balance gasification model, declaring that the whole thermochemical process unequivocally impacts the pyrolysis rate, no matter what the kind of biomass or component utilized. This model explicitly portrays the utilization of one biomass fuel concentrated on a balance model in view of harmony constants to reproduce the gasification cycle in a downdraft gasifier, detailing that the home season of the reactants can be viewed as sufficiently high to arrive at synthetic harmony.

In a significant part of the writing, a couple of specialists have introduced a plan philosophy for downdraft gasifiers, especially zeroing in on huge gasifiers. Outstandingly, there is a critical

hole in writing concerning the plan of downdraft gasifiers more modest than 3.7 kW_e (Fuel input ~14 kW_{th}). This exploration is devoted to tending to this hole by focusing on the plan, improvement, and testing of little downdraft gasifiers with a fuel contribution of under 5 kW_{th}, expected for home-grown cooking applications. The current plan information in the writing doesn't cover this particular power range, requiring the need to make up for this information shortfall. Hence, this work means to foster a far reaching plan strategy for little downdraft gasifiers, trailed by the creation and broad testing of these frameworks. The extent of this examination includes the plan and advancement of the littlest known working downdraft gasifiers inside this power range. The discoveries of this work shed light on the actual peculiarities affecting the rate and degree of gasification, giving bits of knowledge into the circumstances to ideal execution of the gasification framework.

The essential focal point of the ongoing paper is:

- Explore various gasifiers and delve into the critical parameters of gasification.
- Discover the innovative hydrothermal technology as a novel approach to biomass gasification.
- Conduct a comprehensive economic analysis on the gasifiers utilized in the hydrothermal technology for biomass gasification.
- Provide insights into potential future directions in the field, guiding readers towards upcoming developments and opportunities.

2. Gasifiers

2.1 Gasifying medium

Whenever steam has been utilized as a gasifying medium, the gas produced has a larger proportion of H/C [7]. Air is the most frequently utilized gasifying medium for gasification, yet notwithstanding, due to its easy accessibility as well as affordable cost [8]. The focus of McCaffrey et al. [9] was on the use of steam and air in a fluidized bed gasifier at a research centre to gasify almond biomass. They discovered that the presence of steam in the air led to significant hydrogen production and warmth. Yang and Chen [10] supported the increase in hydrogen output by employing oxygen/steam gasification using a downdraft gasifier in order to combat the weakening of syngas by nitrogen, which is typically incorporated during air gasification. In their study, a gasifying specialist uses steam to take care of oxygen. Motta et al. [11] demonstrated the way that oxygen can act as a gasification specialist in their investigation of biomass gasification on rice husk, sawdust, and camphor wood in an entrained-stream gasifier. However, because oxygen is removed from the air using cold and pressure,

oxygen-blown gasification is an energy-intensive and expensive process [12]. Because of its many advantages over conventional gasifying media, supercritical water is a promising gasifying medium that has garnered a lot of attention [12,13]. It is accessible at its supercritical conditions, when there is no distinction between the fluid and gas phases, at 647 K in temperature and 221.2 bar of strain above its basic point [14, 15]. Supercritical water is used as a gasifying medium in an interaction known as supercritical water gasification (SCWG). Surface strain disappears when the two stages overlap at the supercritical point [16].

One major advantage of using SCWG is treating moist biomass feedstock that performs better than every standard cycle [17]. The wet percentage varies from 5% to 35% depending on the biomass feedstock, which absorbs a significant amount of dissipation heat and surpasses the ignition heat obtained via gasification [5,18]. All things considered, the pre-treatment of the feedstock required by the typical gasification process—such as biomass drying—increases the cost of the interaction needlessly [14, 19]. As SCWG is an aqueous interaction, unlike other biomass transformation processes (air/steam/oxygen gasification), excessive water content is not a problem [20]. Despite the hydrogen commitment from biomass, water from SCW also serves as a hydrogen provider and a gasification specialist [21,22,23]. By Examining two studies by Molino et al. [24] and Morris et al. [25], it was discovered that SCWG has great gasification effectiveness at lower temperatures in comparison to other gasification processes, such as air/steam/oxygen gasification. Air has the lowest warming worth represented due to its declining nitrogen content.

2.2 Types of Gasifier

Gasifiers convert stable carbonaceous materials, like biomass or coal, into a gas blend known as syngas (manufactured gas). The sorts of gasifiers rely upon different variables, including the feedstock utilized, working circumstances, and the expected application. Here are a few normal kinds of gasifiers in view of various measures:

1. **Feedstock:**

- **Biomass Gasifiers:** These gasifiers use organic materials such as wood, crop residues, or other plant-based materials as feedstock.
- **Coal Gasifiers:** Designed specifically for coal as the primary feedstock.
- **Municipal Solid Waste (MSW) Gasifiers:** These gasifiers process waste materials to produce syngas.

2. **Operating Temperature:**

- **Fixed-bed Gasifiers:** Operate at relatively lower temperatures and are suitable for solid fuels. Examples include updraft and downdraft gasifiers.
- **Fluidized-bed Gasifiers:** Operate at higher temperatures by suspending the feedstock in an upward-flowing gas or air stream. This includes gasifiers with bubbling and circulating fluidized beds.

3. **Gasification Process:**

- **Updraft Gasifiers:** Under these gasifiers, the reaction zone travels upward through the feedstock bed while the air or gas flows from bottom to top.
- **Downdraft Gasifiers:** The air or gas flows from top to bottom, and the reaction zone moves downward through the bed of feedstock.
- **Crossdraft Gasifiers:** Gasification occurs in a horizontal direction.

4. **Pressure:**

- **Low-Pressure Gasifiers:** Operate at atmospheric pressure or slightly above.
- **High-Pressure Gasifiers:** Operate at elevated pressures, which can enhance the efficiency and improve certain aspects of the gasification process.

5. **Application:**

- **Stationary Gasifiers:** Designed for large-scale, stationary applications such as power plants or industrial facilities.
- **Portable Gasifiers:** Smaller units designed for decentralized or distributed energy generation, suitable for applications like cooking or small-scale power generation in remote areas.

6. **Technology:**

- **Pyrolysis Gasifiers:** It look out for to the feedstock's thermal breakdown in the absence of oxygen.
- **Partial Oxidation Gasifiers:** Entail burning feedstock in part to create syngas.
- **Plasma Gasifiers:** Use high-temperature plasma to convert feedstock into syngas.

The qualities of the feedstock, the planned use of the syngas, the required level of efficiency, and other considerations all have a role in the choice of gasifier type. The choice of a certain type of gasification technology is contingent upon the unique requirements and limitations of a given application. Each gasification technology has pros and cons.

2.3 Gasifier operation

A gasifier typically consists of several distinct zones, each playing a specific role in the gasification process. The key zones in a gasifier are:

- **Drying Zone:** In this zone, the feedstock (such as biomass or coal) is heated to remove moisture. The type of biomass used primarily determines the quality of the product in gasification. regularly, biomass with a wet content of 10% to 20% is suggested for delivering syngas with a high warming worth [26,27]. High-wet content biomass requires drying in the drying zone before gasification. Notwithstanding, the presence of high dampness content prompts energy misfortune and corrupts the item quality [28,29]. The biomass' limited water is changed over into steam over 373 K, and this interaction go on until 473 K [30,31]. Drying is fundamental since wet can obstruct the gasification interaction and diminish in general productivity.
- **Pyrolysis Zone:** The dry feedstock passes through pyrolysis in this zone, which is the heat breakdown of organic molecules without the presence of oxygen. The most unstable substance, hemicellulose, begins to decompose between 423 and 623 K, producing tar, fumes, and scorch [32,33,34]. A temperature of 573 K is suitable if burn formation is the desired outcome. Tracked down in biomass, cellulose degrades at temperatures ranging from 548 to 623 K, producing vaporous products, tar, and fire. However, cellulose yields a significantly higher quantity of tar as compared to hemicellulose. Compared to cellulosic material, lignin produces greater burn when it transforms into aromatics from the lignocellulosic biomass. The temperature range in which lignin decays is 523–773 K [35,36]. Consequently, item selectivity is largely affected by the pyrolysis temperature. Substantial tar is formed over 773 K, and the cycle produces mostly vaporous products and bio-oils [37,38]. Thus, biomass pyrolysis occurs within the range of 398 to 773 K, causing the emergence of various products depending on the selected temperature [39]. This outcomes in the development of unstable mixtures, including tars and gases.
- **Combustion Zone:** Here, a controlled amount of oxygen is introduced to combust a portion of the pyrolysis products. This combustion reaction provides heat for the overall gasification process and helps sustain the necessary high temperatures. However, compared to gasification, the overall intensity released from biomass constituents in the ignition zone is smaller [40]. Exothermic material reactions take place inside the ignition zone, causing a temperature increase between 1373 and 1773 K [41,42,43]. How much gasifying specialist

is normally controlled to keep it from arriving at the debris' slagging temperature, which could cause functional issues [44]. The final products formed in this zone are CO, CO₂, H₂, and H₂O. The intensity released is employed in the pyrolysis cycle and to partially dry the constituents [45].



- **Reduction Zone:** Remaining char and any unburned pyrolysis products react further with gases such as carbon dioxide and water vapor in the reduction zone. An excess of tar in the fuel gas lowers biomass's overall efficiency and increases the plant's overall partition cost [46, 47]. Tar has the potential to block channels and even polymerize into complicated atoms if left untreated [48]. The lower zone gets its name from its ability to reduce the amount of tar particles in the produced gas. They are subjected to a high temperature—roughly 1273 K—to achieve this [49,50]. This stage intends to change over the leftover strong carbon into valuable gases (carbon monoxide and hydrogen) through substance decrease responses.
- **Tar Reforming Step:** This is an additional step focused on reforming tar compounds produced during pyrolysis. Tar reforming helps convert large hydrocarbon molecules into smaller, more manageable hydrocarbons, reducing the risk of tar-related issues in downstream processes.

Understanding and optimizing the conditions in each of these zones are crucial for efficient and effective gasification. Proper control of temperature, residence time, and gas composition in each zone contributes to maximizing the yield of desirable syngas and minimizing unwanted by-products.

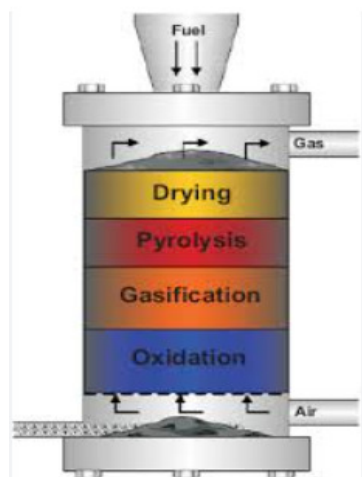


Figure 1. Different zones in gasifier[51]

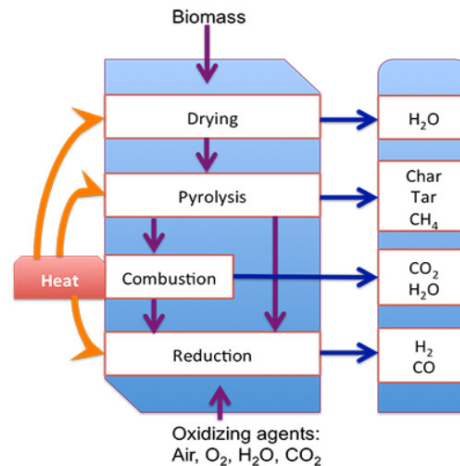


Figure 2. General schematic of different region in the gasifier [52]

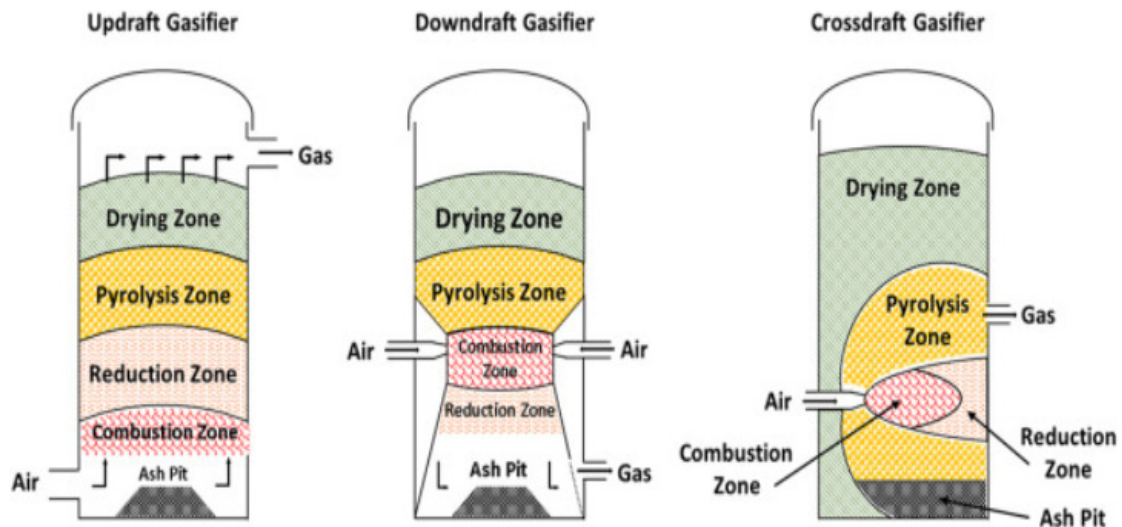


Figure 3. Different types of gasifier [52]

3. CFD Methodology

3.1 Operating parameter

3.1.1 Gasification temperature: The temperature inside the gasifier has an impact on how the syngas are arranged. Higher temperatures generally cause the hydrogen in the syngas to become more concentrated, which is desirable for some uses. Various investigations, including those [53,54] on Ni/BCC and Ni/Al₂O₃ impetuses, have been led to prove this guarantee [55,56]. They investigated tar deterioration coming about because of woody biomass gasification and accomplished reactant tar transforming at a moderately low temperature of 923 K. It's essential to take note of that the ideal gasification temperature relies upon the particular objectives of the gasification cycle, the qualities of the feedstock, and the ideal structure of the syngas.

A crucial aspect of designing and operating a gasification framework is determining an appropriate temperature range. Additionally, kumar et. al. [57] reported the synergistic gasification of bamboo in a fluidized bed. They saw that the tar-changing response was upgraded as the temperature expanded from 400°C to 600°C, involving calcined dolomite as an impetus. Moreover, a diminishing in CO₂ content was noted during the response.

3.1.2 Gasification pressure: Higher pressures in gasifiers are often associated with enhanced gasification reactions and increased gas yields. Operating at elevated pressures can contribute to an improved syngas composition, with increased hydrogen and carbon monoxide

concentrations. Pressure increases cause the supercritical water (SCW) to thicken and the dielectric constant to increase, which speeds up the disruption of biomass [58]. This increased thickness also induces the formation of a shell surrounding the polymerization or coking reactions, which lowers their speeds. This feature has always maintained shifting water-gas shift reactions at high pressure. Furthermore, the thickened layer accelerates the degradation of lignin in biomass [59].

Experiments on the SCWG of rice husk at various stresses (23–34 MPa) and temperatures ranging from 500 to 700°C were conducted [60]. The findings showed that at higher temperatures, strain has a noticeable impact on biomass's SCWG. On the other hand, the SCWG of glycerol and glucose throughout a 5–45 MPa strain range, reasoning that tension insignificantly affected the yield of item gases [61].

3.1.3 Biomass species: [31] investigated the gasification of several biomasses, such as switchgrass, sorghum straw, and red cedar, using various equivalency ratios (ERs).

Red cedar, characterized by its high BET surface area, emerged as a superior feedstock. Specifically, at a low ER ratio, red cedar exhibited a higher heating value (HHV) of 9.09 MJ/kg, although this value decreased with an increase in ER. In a separate study, [62] conducted gasification experiments on lignocellulosic materials and tannery wastes employing the supercritical water (SCW) mechanism. Their results demonstrated the effects of organic components, coke content in the feedstock, and fibrous structure on the yield and composition of gaseous products. Additionally, the moisture content of biomass proved to be a significant factor in gasification. Biomasses with low moisture content (<15 wt%) were deemed suitable for gasifiers. As moisture content increased, the energy requirements showed a proportional variation [63]. Basu [27] undertook a comparative analysis of various biomass feedstocks based on moisture content. The study revealed that wheat straw and rice husk were preferable feedstocks due to their lower moisture content.

3.1.4 Steam- biomass ratio: Keeping an ideal steam-to-biomass proportion inside the prescribed scope of 0.3 to 1.0 essentially impacts the proficiency of this interaction [64]. Examination of different biomass feedstocks, including espresso bean husks, green squanders, food squanders, civil strong squanders, pine sawdust, wood buildup, and wood chips, uncovered an immediate connection between's rising the steam-to-biomass proportion and upgraded hydrogen (H₂) creation. Significantly, greater H₂ concentrations were noted in the

particular steam-to-biomass ratio range of 1.35–4.04 [65]. This emphasizes how important the steam-to-biomass ratio is to maximizing the gasification process's production of H₂.

3.1.5 Equivalence ratio: Increasing the ratio of actual air to fuel in gasification as opposed to the stoichiometric requirement of air to fuel is known as augmenting the equivalency ratio (ER). This addition of more air to the gasifier leads to an elevation in the oxidation reaction rate, resulting in the formation of more CO₂. Sher et al. [66] validated this assertion through gasification experiments with birch-wood feed, where both syngas yield and combustion gasification efficiency (CGE) exhibited an upward trend with increasing ER. Biomass gasification on cellulose highlighted the important impact of ER on product composition in a study [67]. The study found a strong relationship between gasification temperature and ER. The ratio dropped to 2 at a moderate temperature span of 1000–1500 K, whereas optimal ER was found to be 3 in the 600–900 K temperature range. As a result, a drop in ER was linked to an increase in temperature.

3.2 Boundary condition

In ANSYS simulations, a gasifier model would typically involve defining various boundary conditions to accurately represent the physical behaviour of the system. Here are some common boundary conditions you might need to consider for a gasifier simulation. In the context of numerical simulations and finite element analysis, a boundary condition is a set of constraints imposed on a simulation to model the interaction of a system with its external environment. These conditions are essential for solving partial differential equations (PDEs) and obtaining a meaningful and accurate solution. These conditions provide essential information about how the system interacts with its surroundings or adjacent components. Boundary conditions are necessary in many disciplines, such as mathematics, physics, and engineering, in order to solve partial differential equations and characterize how a system reacts to outside stimuli. They can be applied to different types of physical quantities, such as temperature, pressure, velocity, displacement, and concentrations [68]. The choice of boundary conditions depends on the specific problem being simulated and the physical phenomena under consideration.

➤ **Inlet Conditions:**

Specify the composition and temperature of the incoming gases (feedstock) to the gasifier.

➤ **Outlet Conditions:**

Set conditions for the outlet gases, considering the composition, temperature, and pressure of the produced syngas.

➤ **Wall Conditions:**

Define the wall materials and their properties, which can affect heat transfer and reactions occurring within the gasifier.

➤ **Heat Flux or Temperature:**

Apply heat flux or temperature conditions as needed, especially if there are external heat sources or if heat is generated within the gasifier due to chemical reactions.

➤ **Chemical Reactions:**

Include the relevant chemical reactions and their kinetics to simulate the gasification process accurately. This may involve specifying reaction rates, activation energies, and reaction stoichiometry.

➤ **Mass Flow Conditions:**

Set conditions for mass flow rates or mass fractions of different species at various inlets and outlets.

➤ **Pressure Conditions:**

Define pressure conditions, especially at inlets and outlets, to represent the operating pressure of the gasifier.

➤ **Convergence Criteria:**

Specify convergence criteria for the solution. This is crucial for obtaining accurate and reliable results.

➤ **Symmetry or Periodic Conditions:**

If applicable, apply symmetry or periodic conditions to reduce the size of the simulation domain and speed up calculations.

➤ **Initial Conditions:**

Set initial conditions for temperature, pressure, and species concentrations to start the simulation.

For gasifier simulations, always consult the ANSYS manual and any special instructions given. Depending on the particular type of gasifier, the processes involved, and the specifics of the physical setup you are simulating, the precise boundary conditions may change.



Figure 4. mesh analysis



Figure 5. Pressure distribution in the gasifier

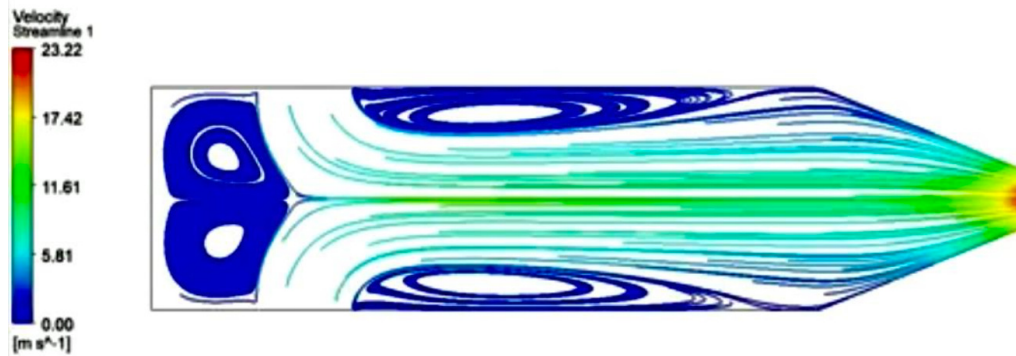


Figure 6. Velocity distribution in the gasifier

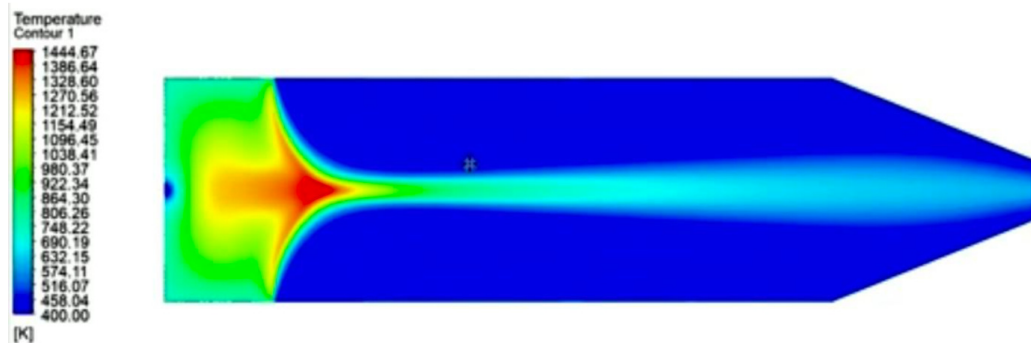


Figure 7. Temperature distribution in the gasifier

4. Application

Gasification technology finds application across various industries and sectors, contributing to sustainable energy production, chemical synthesis, and environmental management. Here are some key applications of gasification technology:

➤ **Power Generation:**

In power plants, gasification is a common method of producing energy. Gasification produces syngas, which can be mixed with steam to create efficient power generation in steam turbines or used in gas turbines.

➤ **Hydrogen Production:**

Gasification can be utilized to produce hydrogen from various feedstocks. Hydrogen is a versatile energy carrier used in industries such as refining, chemicals, and transportation.

➤ **Chemical Synthesis:**

The syngas got from gasification fills in as an important feedstock for the creation of synthetic substances like methanol, smelling salts, and engineered petroleum gas (SNG). These synthetic substances track down applications in different ventures.

➤ **Transportation Fuels:**

Gasification can be used with other processes, such as Fischer-Tropsch synthesis, to produce liquid transportation fuels. This makes it possible to produce synthetic fuels from a range of feedstocks.

➤ **Petrochemical Industry:**

Gasification is employed in the petrochemical industry to convert heavy hydrocarbons and solid wastes into valuable syngas, which can then be used for the production of chemicals and fuels.

5. Challenges and Limitations

➤ **Scale-Up Challenges:**

Scaling up gasification technology from lab-scale or pilot projects to commercial plants can be challenging. Issues related to heat and mass transfer, reactor design, and process control become more pronounced at larger scales.

➤ **Integration with Downstream Processes:**

Efficient integration of gasification with downstream processes, such as syngas cleaning, power generation, or chemical synthesis, requires careful engineering and optimization. Achieving seamless integration poses technical challenges.

➤ **Economic Viability:**

Gasification projects often require significant upfront capital investment. Achieving economic viability, especially when competing with conventional energy sources, remains a challenge. The costs associated with feedstock, equipment, and operation must be carefully managed.

➤ **Environmental Concerns:**

While gasification can be a cleaner alternative to traditional combustion processes, environmental concerns such as emissions of pollutants and the environmental impact of feedstock production must be addressed.

6. Future prospects and conclusion

The utilization of biomass feedstocks for energy generation is a promising solution to the growing scarcity of fossil fuels and the amelioration of worldwide environmental problems. Despite the potential, creating catalysts that are resistant to poisoning, sintering, and coking is proving to be a difficult task for researchers. When it comes to adjusting gasification parameters like temperature, yields of products, and tar formation, catalysts are essential. Another challenge is the successful scale-up following catalyst manufacture. Research is still being done to determine how different catalyst designs affect various reactors under various conditions.

Although our understanding of how catalysts affect biomass gasification has advanced, more may be done to produce catalysts in this area at a lower cost. The efficiency of hydrogen production is also influenced by the type of gasifier or reactor selected, yet current gasifiers are frequently restricted to either small- or large-scale operations. New developments have showed promise in addressing various gasification factors, including twin fluidized bed gasifiers, staged reactors, and downdraft gasifiers with throats.

The copy covers different gasification innovations, with a specific spotlight on Supercritical Water Gasification (SCWG). It investigates key innovations like fixed bed, fluidized bed, and high level gasifiers like entrained stream, double fluidized bed, and SCW reactors. Biomass change is featured as a promising innovation with the possibility to supplant petroleum derivatives, significant in tending to an Earth-wide temperature boost and wellbeing related issues. Fischer-Tropsch (F-T) combination development of biofuels is studied considering constraints such as feedstock type, temperature and strain during operation, home time, and bed material. The text emphasizes the challenges biomass gasification has, such as high energy costs, capital requirements, and total item costs, which limit its use for a wide range of sustainable energy applications. SCWG is introduced as an unrivaled and possibly financially savvy innovation contrasted with other gasifiers, in spite of issues, for example, stopping, effectiveness, erosion, and high hydrogen creation costs. The requirement for future examination is featured, zeroing in on process enhancement, reactor determination, minimal expense impetus planning, and the cautious choice of gasifying medium and innovation to

move the development of biomass energy. The original copy talks about the broad exploration on Ni-based impetuses because of their financial practicality and action. Be that as it may, these impetuses are handily harmed, requiring improvement. Change and interesting earth metals are brought as dopants into Ni-based impetuses to improve their presentation. The requirement for novel impetuses to further develop selectivity, action, and efficiency in biomass gasification is stressed, proposing that further revelations in this space are fundamental for propelling the biomass time.

References

- [1] Najafi, G., Ghobadian, B., Tavakoli, T., Yusaf, T., 2009. *Potential of bioethanol production from agricultural wastes in Iran. Renewable and sustainable energy reviews* 13, 1418-1427.
- [2] Reddy, M.V., Devi, M.P., Chandrasekhar, K., Goud, R.K., Mohan, S.V., 2011. *Aerobic remediation of petroleum sludge through soil supplementation: microbial community analysis. Journal of hazardous materials* 197, 80-87.
- [3] Jahromi, H., Fazelipour, M., Ayatollahi, S., Niazi, A., 2014. *Asphaltenes biodegradation under shaking and static conditions. Fuel* 117
- [4] Spitzley, D.V., Keoleian, G.A., Baron, S.G., 2007. *Life cycle energy and environmental analysis of a microgrid power pavilion. International journal of energy research* 31
- [5] Naqvi, S.R., Uemura, Y., Yusup, S.B., 2014. *Catalytic pyrolysis of paddy husk in a drop type pyrolyzer for bio-oil production: The role of temperature and catalyst. Journal of Analytical and Applied Pyrolysis* 106, 57-62.
- [6] Jahromi, H., Agblevor, F.A., 2017. *Upgrading of pinyon-juniper catalytic pyrolysis oil via hydrodeoxygenation. Energy* 141, 2186-2195
- [7] *Numerical and Experimental Investigation of Equivalence Ratio (ER) and Feedstock Particle Size on Birchwood Gasification. Energies*, 10(8), 1232. doi:10.3390/en10081232(2017).
- [8] X. Hao, L. Guo, X. Zhang, Y. Guan, *Hydrogen production from catalytic gasification of cellulose in supercritical water, Chem. Eng. J.* 110 (1–3) (2005) 57–65, <https://doi.org/10.1016/j.cej.2005.05.002>..
- [9] W. Jangsawang, K. Laohalidanond, S. Kerdsuwan, *Optimum equivalence ratio of biomass gasification process based on thermodynamic equilibrium model, Energy Procedia* 79 (2015) 520–527, <https://doi.org/10.1016/j.egypro.2015.11.528>.

- [10] Yang, H., & Chen, H. (2015). Biomass gasification for synthetic liquid fuel production. *Gasification for Synthetic Fuel Production*, 241–275. DOI:10.1016/b978-0-85709-802-3.00011-4
- [11] I.L. Motta, N.T. Miranda, R. Maciel Filho, M.R. Wolf Maciel, Biomass gasification in fluidized beds: A review of biomass moisture content and operating pressure effects, *Renew. Sustain. Energy Rev.* 94 (2018) 998–1023, <https://doi.org/10.1016/j.rser.2018.06.042>.
- [12] A. Molino, S. Chianese, D. Musmarra, Biomass gasification technology: the state of the art overview, *J Energy Chem* 2016 (25) (2016) 10–25, <https://doi.org/10.1016/j.jechem.2015.11.005>.
- [13] A. Molino, S. Chianese, D. Musmarra, Biomass gasification technology: the state of the art overview, *J Energy Chem* 2016 (25) (2016) 10–25, <https://doi.org/10.1016/j.jechem.2015.11.005>.
- [14] C. Xu, J. Donald, E. Byambajav, Y. Ohtsuka, Recent advances in catalysts for hot-gas removal of tar and NH₃ from biomass gasification, *Fuel* 89 (8) (2010) 1784–1795, <https://doi.org/10.1016/j.fuel.2010.02.014>.
- [15] V.S. Sikarwar, M. Zhao, P.S. Fennell, N. Shah, E.J. Anthony, Progress in biofuel production from gasification, *Prog. Energy Combust. Sci.* 61 (2017) 189–248, <https://doi.org/10.1016/j.pecs.2017.04.001>.
- [16] M.L. Valderrama Rios, A.M. González, E.E.S. Lora, O.A. Almazán del Olmo, Reduction of tar generated during biomass gasification: A review, *Biomass Bioenergy* 108 (2018) 345–370, <https://doi.org/10.1016/j.biombioe.2017.12.002>.
- [17] Z. McCaffrey, P. Thy, M. Long, M. Oliveira, L. Wang, L. Torres, T. Aktas, B.-S. Chiou, W. Orts, B.M. Jenkins, Air and steam gasification of almond biomass, *Front. Energy Res.* 7 (2019) 84, <https://doi.org/10.3389/fenrg.2019.00084>.
- [18] D.D. Gray, Major gasifiers for IGCC systems, *Integrated Gasification Combined Cycle (IGCC) Technologies* (2017) 305–355, <https://doi.org/10.1016/b978-0-08-100167-7.00008-1>
- [19] R. Warnecke, Gasification of biomass: comparison of fixed bed and fluidized bed gasifier, *Biomass Bioenergy* 18 (6) (2000) 489–497, [https://doi.org/10.1016/s0961-9534\(00\)00009-x](https://doi.org/10.1016/s0961-9534(00)00009-x).
- [20] X. Meng, W. de Jong, N. Fu, A.H.M. Verkooijen, Biomass gasification in a 100 kWth steam-oxygen blown circulating fluidized bed gasifier: Effects of operational conditions

- on product gas distribution and tar formation, *Biomass Bioenergy* 35 (7) (2011) 2910–2924, <https://doi.org/10.1016/j.biombioe.2011.03.028>.
- [21] M. Siedlecki, W. De Jong, A.H.M. Verkooijen, *Fluidized bed gasification as a mature and reliable technology for the production of bio-syngas and applied in the production of liquid transportation fuels—A review*, *Energies* 4 (3) (2011) 389–434, <https://doi.org/10.3390/en4030389>.
- [22] R. Thomson, P. Kwong, E. Ahmad, K.D.P. Nigam, *Clean syngas from small commercial biomass gasifiers; a review of gasifier development, recent advances and performance evaluation*, *Int. J. Hydrogen Energy* 45 (41) (2020) 21087–21111, <https://doi.org/10.1016/j.ijhydene.2020.05.160>.
- [23] D. Hantoko, H. Su, M. Yan, E. Kanchanatip, H. Susanto, G. Wang, S. Zhang, Z. Xu, *Thermodynamic study on the integrated supercritical water gasification with reforming process for hydrogen production: Effects of operating parameters*, *Int. J. Hydrogen Energy* 43 (37) (2018) 17620–17632, <https://doi.org/10.1016/j.ijhydene.2018.07.198>.
- [24] A. Molino, V. Larocca, S. Chianese, D. Musmarra, *Biofuels production by biomass gasification: A review*, *Energies* 11 (4) (2018) 811, <https://doi.org/10.3390/en11040811>.
- [25] J.D. Morris, S.S. Daood, S. Chilton, W. Nimmo, *Mechanisms and mitigation of agglomeration during fluidized bed combustion of biomass: A review*, *Fuel* 230 (2018) 452–473, <https://doi.org/10.1016/j.fuel.2018.04.098>.
- [26] M. Siedlecki, R. Nieuwstraten, E. Simeone, W. de Jong, A.H.M. Verkooijen, *Effect of magnesite as bed material in a 100 kWth steam oxygen blown circulating fluidized-bed biomass gasifier on gas composition and tar formation*, *Energy Fuels* 23 (11) (2009) 5643–5654, <https://doi.org/10.1021/ef900420c>.
- [27] P. Basu, *Biomass Gasification and Pyrolysis: Practical Design and Theory*, Elsevier, Chichester, 2010, p. 1.
- [28] Niaounakis M., Halvadakis C.P. (2006). Chapter 10- Uses. *Waste Management Series*, 5, 235-292. [https://doi.org/10.1016/S0713-2743\(06\)80012-7](https://doi.org/10.1016/S0713-2743(06)80012-7)
- [29] Basu P. (2013). *Biomass Gasification, Pyrolysis, and Torrefaction Practical Design and Theory Second Edition*. AP. pp: 548.
- [30] Wheeldon, J. M., & Thimsen, D. (2013). *Economic evaluation of circulating fluidized bed combustion (CFBC) power generation plants. Fluidized Bed Technologies for Near-Zero Emission Combustion and Gasification*, 620–638. doi:10.1533/9780857098801.2.620

- [31] K. Qian, A. Kumar, K. Patil, D. Bellmer, D. Wang, W. Yuan, R. Huhnke, *Effects of biomass feedstocks and gasification conditions on the physiochemical properties of char*, *Energies* 6 (8) (2013) 3972–3986, <https://doi.org/10.3390/en6083972>.
- [32] P. Lv, Z. Yuan, L. Ma, C. Wu, Y. Chen, J. Zhu, *Hydrogen-rich gas production from biomass air and oxygen/steam gasification in a downdraft gasifier*, *Renewable Energy* 32 (13) (2007) 2173–2185, <https://doi.org/10.1016/j.renene.2006.11.010>
- [33] J. Zhou, Q. Chen, H. Zhao, X. Cao, Q. Mei, Z. Luo, K. Cen, *Biomass–oxygen gasification in a high-temperature entrained-flow gasifier*, *Biotechnol. Adv.* 27 (5) (2009) 606–611, <https://doi.org/10.1016/j.biotechadv.2009.04>.
- [34] Choudhury, H. A., Chakma, S., & Moholkar, V. S. (2015). *Biomass Gasification Integrated Fischer-Tropsch Synthesis. Recent Advances in Thermo-Chemical Conversion of Biomass*, 383–435. DOI:10.1016/b978-0-444-63289-0.00014-4
- [35] S. Pang, *Chapter – 9 Fuel flexible gas production: Biomass, coal and bio-solid wastes*, *Fuel Flex. Energy Gener. Solid Liquid Gaseous Fuels* (2016) 241–269, <https://doi.org/10.1016/B978-1-78242-378-2.00009-2>.
- [36] A. Bhattacharya, A. Datta, *Modeling of hydrogen production process from biomass using oxygen blown gasification*, *Int. J. Hydrogen Energy* 37 (24) (2012) 18782–18790, <https://doi.org/10.1016/j.ijhydene.2012.09.13>.
- [37] Y. Chhiti, M. Kemiha, *Thermal Conversion of biomass, pyrolysis and gasification: A review*, *Int. J. Eng. Sci. (IJES)* 2 (3) (2013) 75–85
- [38] Gomez-Barea A, Bl, Ollero P. (2011). *Methods to improve the performance of fluidized bed biomass gasifiers. In: Paper presented at: 2nd European conference on polygeneration, [Tarragona, Spain]*.
- [39] E.D. Gemechu, A. Kumar, *Chapter 12 - The Environmental Performance Of Hydrogen Production Pathways Based On Renewable Sources, Renewable Energy-Driven Future Technologies, Modelling, Applications, Sustainability and Policies, 2021*, pp. 375–406
- [40] J. Zhou, Q. Chen, H. Zhao, X. Cao, Q. Mei, Z. Luo, K. Cen, *Biomass-oxygen gasification in a high-temperature entrained-flow gasifier*, *Biotechnol. Adv.* 27 (5) (2009) 606–611, <https://doi.org/10.1016/j.biotechadv.2009.04.011>.
- [41] W.-H. Chen, C.-J. Chen, C.-I. Hung, C.-H. Shen, H.-W. Hsu, *A comparison of gasification phenomena among raw biomass, torrefied biomass and coal in an entrained-flow reactor*, *Appl. Energy* 112 (2013) 421–430, <https://doi.org/10.1016/j.apenergy.2013.01.034>.

- [42] Y. Guo, S.Z. Wang, D.H. Xu, Y.M. Gong, H.H. Ma, X.Y. Tang, *Review of catalytic supercritical water gasification for hydrogen production from biomass*, *Renew. Sustain. Energy Rev.* 14 (1) (2010) 334–343, <https://doi.org/10.1016/j.rser.2009.08.012>.
- [43] O. Yakaboylu, J. Harinck, K. Smit, W. de Jong, *Supercritical water gasification of biomass: A literature and technology overview*, *Energies* 8 (2) (2015) 859–894, <https://doi.org/10.3390/en8020859>.
- [44] Y. Zhao, S. Sun, H. Zhou, R. Sun, H. Tian, J. Luan, J. Qian, *Experimental study on sawdust air gasification in an entrained-flow reactor*, *Fuel Process. Technol.* 91 (8) (2010) 910–914, <https://doi.org/10.1016/j.fuproc.2010.01.012>.
- [45] https://www.researchgate.net/figure/Fixed-bed-updraft-gasifier_fig1_266292799
- [46] J.A. Okolie, R. Rana, S. Nanda, A.K. Dalai, J.A. Kozinski, *Supercritical water gasification of biomass: a state-of-the-art review of process parameters, reaction mechanisms and catalysis*, *Sustainable Energy Fuels* 3 (3) (2019) 578–598, <https://doi.org/10.1039/C8SE00565F>.
- [47] R.F. Susanti, J. Kim, K. Yoo, *Supercritical Water Gasification for Hydrogen Production. Supercritical Fluid Technology for Energy and Environmental Applications*, Elsevier, 2014, pp. 111–137, 10.1016/B978-0-444-62696-7.00006-X.
- [48] Y. Hu, M. Gong, X. Xing, H. Wang, Y. Zeng, C.C. Xu, *Supercritical water gasification of biomass model compounds: A review*, *Renew. Sustain. Energy Rev.* 118 (2020) 109529, <https://doi.org/10.1016/j.rser.2019.109529>.
- [49] S.N. Reddy, S. Nanda, A.K. Dalai, J.A. Kozinski, *Supercritical water gasification of biomass for hydrogen production*, *Int. J. Hydrogen Energy* 39 (13) (2014) 6912–6926, <https://doi.org/10.1016/j.ijhydene.2014.02.125>.
- [50] S.K. Sansaniwal, K. Pal, M.A. Rosen, S.K. Tyagi, *Recent advances in the development of biomass gasification technology: A comprehensive review*, *Renew. Sustain. Energy Rev.* 72 (2017) 363–384, <https://doi.org/10.1016/j.rser.2017.01.038>.
- [51] <https://www.e-education.psu.edu/egee439/node/607>
- [52] <https://www.sciencedirect.com/topics/engineering/fixed-bed-gasifiers>
- [53] Huber, G.W., Iborra, S., Corma, A., 2006. *Synthesis of transportation fuels from biomass: chemistry, catalysts, and engineering*. *Chemical reviews* 106, 4044–4098.
- [54] Y. Matsumura, *Evaluation of supercritical water gasification and biomethanation for wet biomass utilization in Japan*, *Energy Convers. Manage.* 43 (9–12) (2002) 1301–1310, [https://doi.org/10.1016/s0196-8904\(02\)00016-x](https://doi.org/10.1016/s0196-8904(02)00016-x).

- [55] D. Hantoko, M. Yan, B. Prabowo, H. Susanto, X. Li, C. Chen, *Aspen Plus Modeling Approach in Solid Waste Gasification, Current Developments in Biotechnology and Bioengineering, Waste Treatment Processes for Energy Generation*, 2019, pp. 259–281.
- [56] Karmee, S.K., Swanepoel, W., Marx, S., 2018. *Biofuel production from spent coffee grounds via lipase catalysis. Energy Sources, Part A: Recovery, Utilization, and Environmental Effects* 40, 294-300
- [57] A. Kumar, K. Eskridge, D.D. Jones, M.A. Hanna, *Steam–air fluidized bed gasification of distillers grains: Effects of steam to biomass ratio, equivalence ratio and gasification temperature, Bioresour. Technol.* 100 (6) (2009) 2062– 2068, <https://doi.org/10.1016/j.biortech.2008.10.011>.
- [58] Nanda, S., Azargohar, R., Dalai, A.K., Kozinski, J.A., 2015. *An assessment on the sustainability of lignocellulosic biomass for biorefining. Renewable and sustainable energy reviews* 50, 925-941.
- [59] E. Shayan, V. Zare, I. Mirzaee, *Hydrogen production from biomass gasification; a theoretical comparison of using different gasification agents, Energy Convers. Manage.* 159 (2018) 30–41, <https://doi.org/10.1016/j.enconman.2017.12.09>.
- [60] Hakeem, K.R., Jawaid, M., Allothman, O.Y., 2015. *Agricultural biomass based potential materials. Springer*
- [61] Q. Yan, L. Guo, Y. Lu, *Thermodynamic analysis of hydrogen production from biomass gasification in supercritical water, Energy Convers. Manage.* 47 (11– 12) (2006) 1515– 1528, <https://doi.org/10.1016/j.enconman.2005.08.00>.
- [62] Zaman, C. Z., Pal, K., Yehye, W. A., Sagadevan, S., Shah, S. T., Adebisi, G. A., ... Johan, R. B. (2017). *Pyrolysis: A Sustainable Way to Generate Energy from Waste. Pyrolysis.* doi:10.5772/intechopen.69036
- [63] Kirubakaran, V., Sivaramakrishnan, V., Nalini, R., Sekar, T., Premalatha, M., Subramanian, P., 2009. *A review on gasification of biomass. Renewable and sustainable energy reviews* 13, 179-186.
- [64] Chogani, A., Moosavi, A., Rahiminejad, M., 2016. *Numerical Simulation of Salt Water Passing Mechanism Through Nanoporous Single-Layer Graphene Membrane. Chemical Product and Process Modeling* 11, 73-76
- [65] R.Z. Vigouroux, *Pyrolysis of Biomass- Dissertation, Royal Institute of Technology, 2001.*
- [66] F. Sher, M.A. Pans, C. Sun, C. Snape, H. Liu, *Oxy-fuel combustion study of biomass fuels in a 20 kWth fluidized bed combustor, Fuel* 215 (2018) 778– 786, <https://doi.org/10.1016/j.fuel.2017.11.039>.

- [67] A. Kumar, D. Jones, M. Hanna, *Thermochemical biomass gasification: A review of the current status of the technology*, *Energies* 2 (3) (2009) 556–581, <https://doi.org/10.3390/en20300556>.
- [68] Patra, T.K., Sheth, P.N., 2015. *Biomass gasification models for downdraft gasifier: A state-of-the-art review*. *Renewable and sustainable energy reviews* 50, 583-593.
- [69] Sharzehee, M., Khalafvand, S.S., Han, H.-C., 2018. *Fluid-structure interaction modeling of aneurysmal arteries under steady-state and pulsatile blood flow: A stability analysis*. *Computer methods in biomechanics and biomedical engineering* 21, 219-231.
- [70] A. Mishra, S. Gautam, T. Sharma, *Effect of operating parameters on coal gasification*, *Int. J. Coal Sci. Technol.* 5 (2) (2018) 113–125, <https://doi.org/10.1007/s40789-018-0196-3>.
- [71] Wang, Y., Kinoshita, C., 1993. *Kinetic model of biomass gasification*. *Solar Energy* 51, 19-25.
- [72] Sharma, A.K., 2008. *Equilibrium modeling of global reduction reactions for a downdraft (biomass) gasifier*. *Energy Conversion and Management* 49, 832-842.
- [73] Zainal, Z., Ali, R., Lean, C., Seetharamu, K., 2001. *Prediction of performance of a downdraft gasifier using equilibrium modeling for different biomass materials*. *Energy Conversion and Management* 42, 1499-1515
- [74] Hofbauer H, Materazzi M. (2019). *Chapter 7-Waste gasification processes for SNG production*. *Substitute Natural Gas from Waste*. pp: 105-160.
- [75] A. Dassey, B. Mukherjee, R. Sheffield, C. Theegala, *Catalytic cracking of tars from biomass gasification*, *Biomass Convers. Biorefin.* 3 (2) (2012) 69–77, <https://doi.org/10.1007/s13399-012-0063-1>.
- [76] V.S. Sikarwar, M. Zhao, P. Clough, J. Yao, X. Zhong, M.Z. Memon, N. Shah, E.J. Anthony, P.S. Fennell, *An overview of advances in biomass gasification*, *Energy Environ. Sci.* 9 (10) (2016) 2939–2977, <https://doi.org/10.1039/C6EE00935B>.
- [77] Park CS, Roy PS, Kim SH. (2018). *Current Developments in Thermochemical Conversion of Biomass to Fuels and Chemicals*. *Gasification for Low-grade Feedstock*, Yongseung Yun, IntechOpen, DOI: 10.5772/intechopen.71464.
- [78] L. Guo, C. Cao, Y. Lu, *Supercritical water gasification of biomass and organic wastes*, *Biomass* (2010), <https://doi.org/10.5772/9774>
- [79] C. Srinivasakannan, N. Balasubramanian, *Variations in the design of dual fluidized bed gasifiers and the quality of syngas from biomass*, *Energy Sources Part A* 33 (4) (2010) 349–359, <https://doi.org/10.1080/15567030902967835>.

- [80] P. Basu, V. Mettanant, *Biomass Gasification in Supercritical Water – A Review*, *Int. J. Chem. Reactor Eng.* 7 (1) (2009), <https://doi.org/10.2202/1542-6580.1919>.
- [81] Duc, L., Morishita, K., & Takar, T. (2013). *Catalytic Decomposition of Biomass Tars at Low-Temperature*. *Biomass Now - Sustainable Growth and Use*. DOI: 10.5772/55356
- [82] A. Kruse, *Supercritical water gasification*, *Biofpr: Biofuels Bioproducts, Biorefining*. 2 (5) (2008) 415–437, <https://doi.org/10.1002/bbb.v2:510.1002/bbb.93>.
- [83] J. Ren, J.-P. Cao, X.-Y. Zhao, F.-L. Yang, X.-Y. Wei, *Recent advances in syngas production from biomass catalytic gasification: A critical review on reactors, catalysts, catalytic mechanisms and mathematical models*, *Renew. Sustain. Energy Rev.* 116 (2019) 109426, <https://doi.org/10.1016/j.rser.2019.109426>.